Commercial Water Heating Using Gas Absorption Heat Pumps

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Topics of Discussion

- GAHP Technology Background
- GAHP Development Status
- Energy Use Modeling: Full-Service Restaurant
 - Engineering Equation Solver (SMTI)
 - EnergyPlus (ORNL)





Commercial Water Heating Uses Significant Energy

- ❖ 7% U.S. Commercial Energy Use (1.2 Quads)
- 9% Canadian Commercial Energy Use
- **❖** 5.5% U.S. Commercial Sector CO₂ Emissions

Source: US DOE and NRCAN

Commercial Gas Water Heating Equipment

Thermal Efficiency

(1.3 - 1.6 COP)

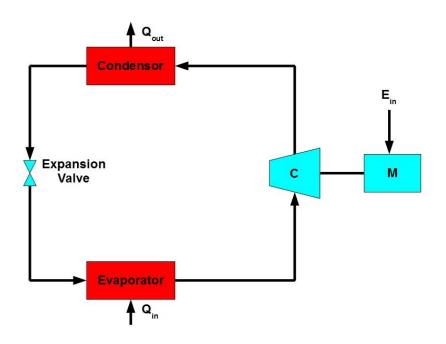
Efficiency

❖ Non-Condensing:
80 - 82%

❖ Condensing: 90 − 95% +15%

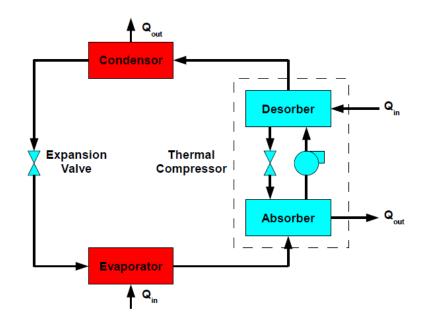
❖ Gas Absorption Heat Pump 130 - 160% +70%

How Does It Work?



$$COP_h = Qcond/E_{in} = 3.0-4.0$$

Qheat = ~1.2 x Qevap

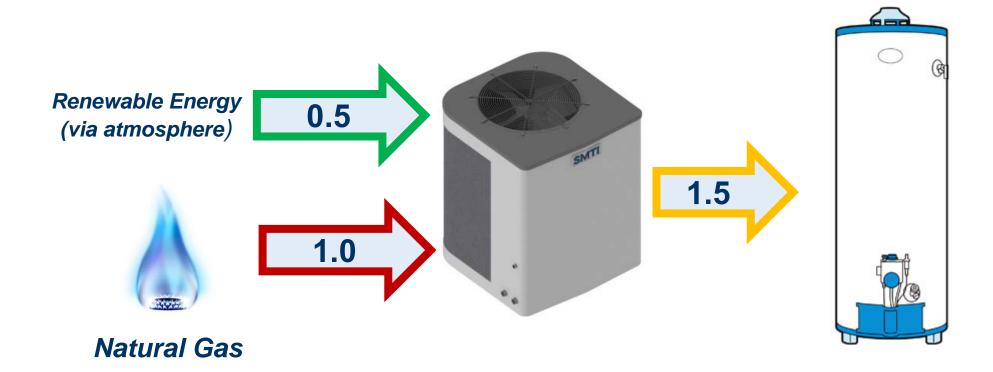


$$COP_h = (Qcond + Qabs)/Q_{in} = 1.4-2.0$$

Qheat = (Qcond + Qabs) ~ 2.5 times Qevap

Capacity & COP Remain High at Low Ambient Temperatures

Gas Absorption's Renewable Energy Content: 35%



SMTI Gas Absorption Heat Pumps



$COP_{HHV} = 1.4 \text{ at } 47/120^{\circ}F$

- Gas-Fired, Air to Water Heat Pump
- Condensing
- ❖ 4:1 Modulation
- **❖ 10,000 to 140,000 Bth Heating Output Models**
- 20° F Hydronic Differential
- Outdoor Installation (no venting)
- SCAQMD NOx Compliant



GAHP Development Status

10,000 btu/hr



140,000 btu/hr



Field Testing



Field Testing



Lab Testing









Energy Use Simulations - Preliminary Results

1. Using Engineering Equation Solver (SMTI)*

Case 1: 2080 gpd

Case 2: 4060 gpd

2. Using EnergyPlus (ORNL)

Case 1: 2080 gpd

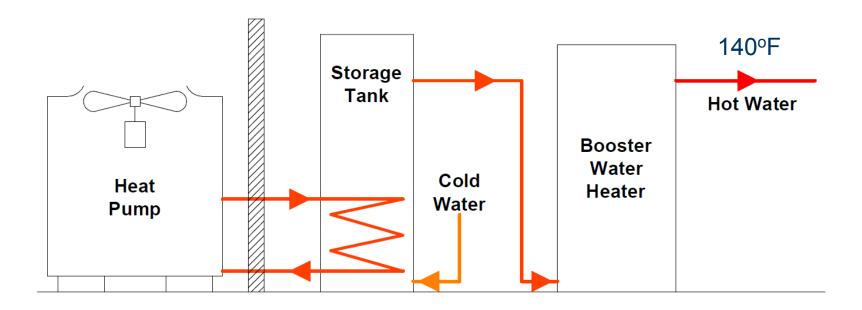
199 kBth Cond Storage + 199 kBth NC Storage Vs.

140 kBth GAHP + 199 kBth NC Storage

^{*} Dr. Chris Keinath

GAHP Commercial Water Heating

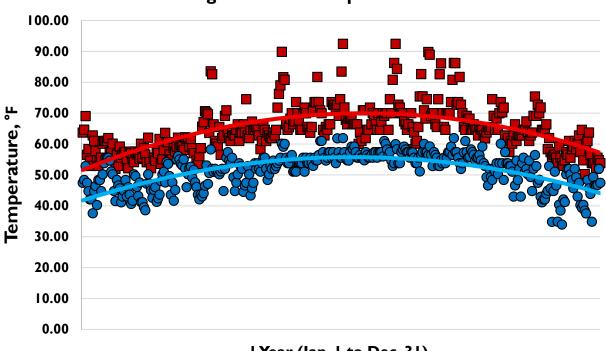
Pre-Heater Installation



Ambient Temperature from Energy Plus

Oakland, California

Ambient High and Low Temperature for Year

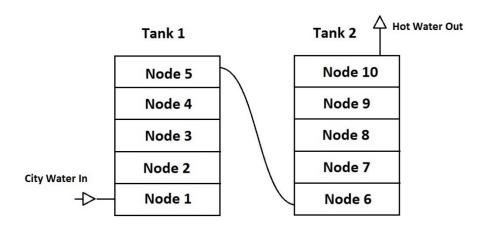


I Year (Jan. I to Dec. 31)

Yearly Average: 58°F

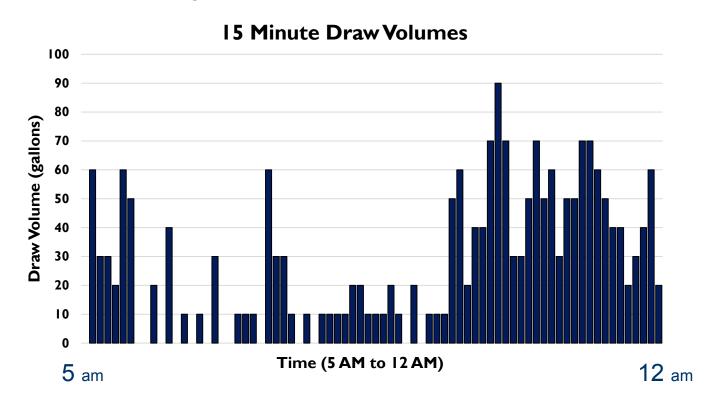
Engineering Equation Solver Model: Assumptions

- A hot water draw happens at the start of each 15 minute period
- Water is drawn into the bottom of Tank 1 at 54.7°F
- Water exiting the top of Tank 1 enters the bottom of Tank 2
- COP for the GAHP and Condensing units use <u>average</u> bottom node temperature for each 15 minute step
- Modulation is neglected
- ❖ GAHP electrical load of 900 W, Condensing unit electrical load of 150 W



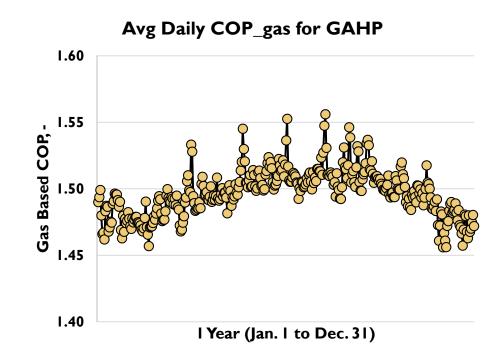
Commercial Water Heating: Case 1 Simulated Draw Pattern

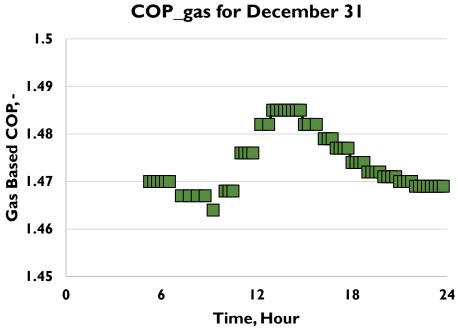
Full Service Restaurant - Daily draw pattern Daily use: 2080 Gallons of Hot Water



Note: Draw pattern for FSR approximated from data presented by: Pacific Gas and Electric. 2007b. *Energy Efficiency Potential of Gas-Fired Commercial Hot Water Heating Systems in Restaurants: An Emerging Technology Field Monitoring Study.* FSTC Report 5011.07.04. San Ramon, CA.

Commercial Water Heating: Case 1 *GAHP Performance*





Commercial Water Heating: Case 1 GAHP Pre-Heat

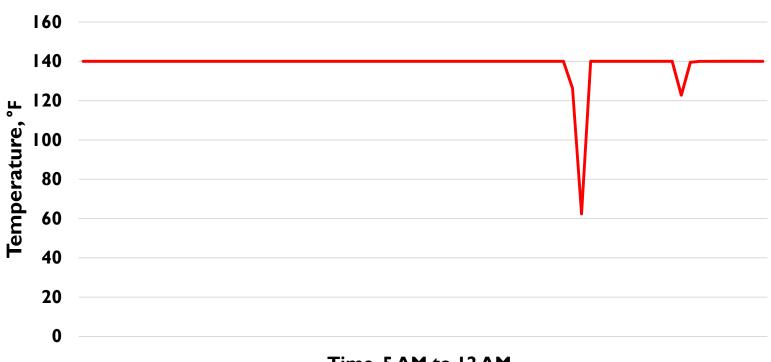
GAHP Avg. Gas COP of 1.53

140 kbtu/hr GAHP Tank unit and 199 kbtu/hr Standard Tank Unit ,2 x 100 gallon tanks								
Tank 1 (GAHP)					Tank 2 (NC)			
Gas Used	Electricity Used	Cost of Gas	Cost of Electricity	Gas Used	Electricity Used	Cost of Gas	Cost of Electricity	
Therms	kWh	\$	\$	Therms	kWh	\$	\$	
282	432	\$282	\$52	7.4	0	\$7	\$0	
256	391	\$256	\$47	6.9	0	\$7	\$0	
281	432	\$281	\$52	7.1	0	\$7	\$0	
271	419	\$271	\$50	6.6	0	\$7	\$0	
279	432	\$279	\$52	6.6	0	\$7	\$0	
269	419	\$269	\$50	6.2	0	\$6	\$0	
278	432	\$278	\$52	6.5	0	\$6	\$0	
278	432	\$278	\$52	6.3	0	\$6	\$0	
269	419	\$269	\$50	6.0	0	\$6	\$0	
280	432	\$280	\$52	6.8	0	\$7	\$0	
272	419	\$272	\$50	6.8	0	\$7	\$0	
283	432	\$283	\$52	7.8	0	\$8	\$0	
3299	5092	\$3,299	\$611	81.0	0.00	\$81	\$0	
Total Operating Cost		\$3,991						
	Gas Used Therms 282 256 281 271 279 269 278 278 269 280 272 283 3299	Tank 1 Gas Used Electricity Therms kWh 282 432 256 391 281 432 271 419 279 432 269 419 278 432 269 419 280 432 272 419 283 432 3299 5092	Tank 1 (GAHP) Gas Used Electricity Used Cost of Gas Therms kWh \$ 282 432 \$282 256 391 \$256 281 432 \$281 271 419 \$271 279 432 \$279 269 419 \$269 278 432 \$278 269 419 \$269 280 432 \$280 272 419 \$272 283 432 \$283 3299 5092 \$3,299	Tank 1 (GAHP) Gas Used Electricity Used kWh \$ \$ 282 432 \$282 \$52 256 391 \$256 \$47 281 432 \$281 \$52 271 419 \$271 \$50 279 432 \$279 \$52 269 419 \$269 \$50 278 432 \$278 \$52 278 432 \$278 \$52 269 419 \$269 \$50 280 432 \$280 \$52 272 419 \$272 \$50 283 432 \$283 \$52 3299 5092 \$3,299 \$611	Tank 1 (GAHP) Gas Used Electricity Used Vused Cost of Gas Electricity Gas Used Electricity Therms kWh \$ \$ 282 432 \$282 \$52 7.4 256 391 \$256 \$47 6.9 9 281 432 \$281 \$52 7.1 6.9 7.1 7.2 7.1 7.2 7.1 7.2 7.1 7.2 7.2 7.2 7.2 7.2 7.2 7.2 7.2 7.2 7.2 7.2 7.2 7.2 <	Tank 1 (GAHP) Tank Gas Used Electricity Used Cost of Gas Electricity Cost of Electricity Gas Used KWh Electricity Used KWh 282 432 \$282 \$52 7.4 0 256 391 \$256 \$47 6.9 0 281 432 \$281 \$52 7.1 0 271 419 \$271 \$50 6.6 0 279 432 \$279 \$52 6.6 0 269 419 \$269 \$50 6.2 0 278 432 \$278 \$52 6.3 0 278 432 \$278 \$52 6.3 0 280 432 \$280 \$52 6.8 0 280 432 \$280 \$52 6.8 0 283 432 \$283 \$52 7.8 0	Tank 1 (GAHP) Tank 2 (NC) Gas Used Electricity Used Cost of Electricity Gas Used Electricity Used Cost of Used Gas Therms kWh \$ \$ Therms kWh \$ 282 432 \$282 \$52 7.4 0 \$7 256 391 \$256 \$47 6.9 0 \$7 281 432 \$281 \$52 7.1 0 \$7 281 432 \$281 \$52 7.1 0 \$7 271 419 \$271 \$50 6.6 0 \$7 279 432 \$279 \$52 6.6 0 \$7 269 419 \$269 \$50 6.2 0 \$6 278 432 \$278 \$52 6.5 0 \$6 280 419 \$269 \$50 6.0 0 \$6 280 432 \$280 \$52	

Note: Assumed cost of Natural Gas – \$1.00/therm, Electricity \$0.12/kWh

Commercial Water Heating: Case 1





Time, 5 AM to 12 AM

Commercial Water Heating: Case 1 Condensing + Non-Condensing

	Tank 1 (Condensing)				Tank 2 (NC)			
Month	Gas Used	Electricity Used	Cost of Gas	Cost of Electricity	Gas Used	Electricity Used	Cost of Gas	Cost of Electricity
	Therms	kWh	\$	\$	Therms	kWh	\$	\$
January	459	72	\$459	\$9	1.6	0	\$2	\$0
February	414	65	\$414	\$8	1.5	0	\$1	\$0
March	459	72	\$459	\$9	1.6	0	\$2	\$0
April	444	70	\$444	\$8	1.6	0	\$2	\$0
May	459	72	\$459	\$9	1.6	0	\$2	\$0
June	444	70	\$444	\$8	1.6	0	\$2	\$0
July	459	72	\$459	\$9	1.6	0	\$2	\$0
August	459	72	\$459	\$9	1.6	0	\$2	\$0
September	444	70	\$444	\$8	1.6	0	\$2	\$0
October	459	72	\$459	\$9	1.6	0	\$2	\$0
November	444	70	\$444	\$8	1.6	0	\$2	\$0
December	459	72	\$459	\$9	1.6	0	\$2	\$0
Total	5401	849	\$5,401	\$102	19.0	0.00	\$19	\$0
	Total Ope	rating Cost	\$5,522					

Note: Assumed cost of Natural Gas – \$1.00/therm, Electricity \$0.12/kWh

Commercial Water Heating: Case 1 Comparison between Condensing and GAHP Pre-Heat

		Condensing Pre-Heat	GAHP Pre-Heat	Annual Savings	% Difference
Total Natural Gas Used	Therms	5,420	3,380	2,040	38%
Cost of Gas Used	\$	\$5,420	\$3,380	\$2,040	38%
Total Electricity Used	kWh	849	5,092	-4,243	
Cost of Electricity Used	\$	\$102	\$611	-\$509	
Total Energy Used	kWh	159,665	104,123	55,542	35%
Total Primary Energy Used	kWh	175,783	123,983	51,800	29%
Annual Operating Cost	\$	\$5,522	\$3,991	\$1,531	28%

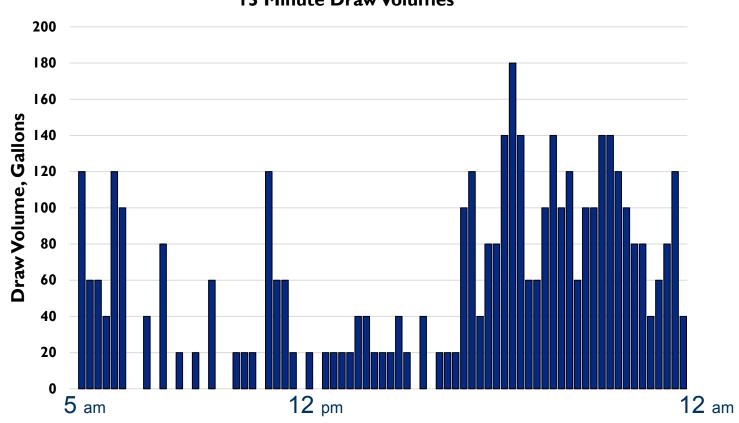
Note: For Primary Energy Conversion: Electric use multiplied by 3.15, Gas use multiplied by 1.09

Natural Gas = \$1.00/therm Electricity = \$0.12/kWhr

Commercial Water Heating: Case 2 Simulated Draw Pattern

Daily use: 4160 Gallons of Hot Water





Commercial Water Heating *Case 2 Exiting Water Temperature (4160 gpd)*

Water Temperature Exiting GAHP Coupled Tank



Commercial Water Heating: Case 2 Comparison between Condensing and GAHP Pre-Heat

		Condensing Pre-Heat	GAHP Pre-Heat	Annual Savings	% Difference
Total Natural Gas Used	Therms	10,934	7,895	3,039	28%
Cost of Gas Used	\$	\$10,934	\$7,895	\$3,039	28%
Total Electricity Used	kWh	876	5,420	-4,544	
Cost of Electricity Used	\$	\$105	\$650	-\$545	
Total Energy Used	kWh	321,229	236,737	84,492	26%
Total Primary Energy Used	kWh	351,944	269,209	82,735	24%
Annual Operating Cost	\$	\$11,039	\$8,545	\$2,493	23%

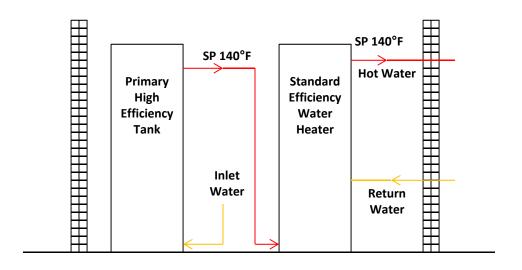
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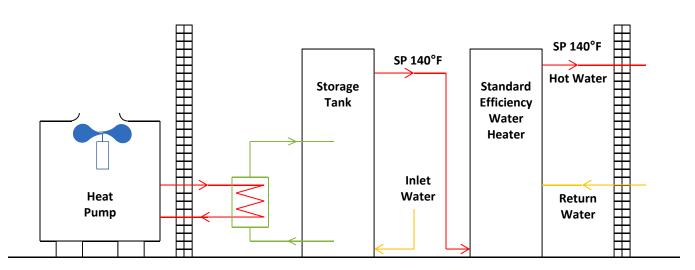
Natural Gas = \$1.00/therm Electricity = \$0.12/kWhr

Energy Plus Modeling

Oak Ridge National Lab

System Configurations







System Assumptions

GAHP

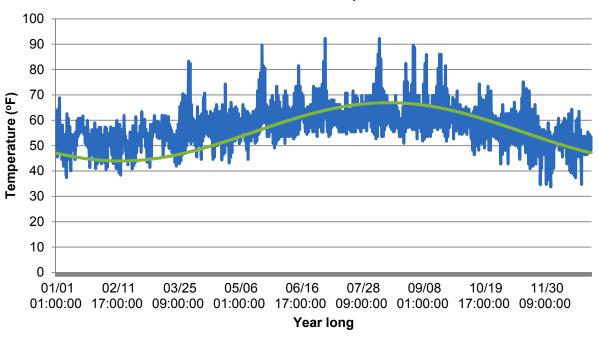
- WaterHeater:HeatPump
- WaterHeater:Stratified
- COP related to the ambient air and mains hydronic temperature
- Second tank 80% efficient
- Set Point 140 °F
- Oakland, CA
- Full service restaurant

Condensing Tank Pre-Heat

- WaterHeater:Stratified
- COP ranging from 98% to 82% depending on Flue Gas Exit Temperature (assumed node 6)
- Second tank 80% efficient
- Set Point 140 °F
- Oakland, CA
- Full service restaurant



Ambient Air and Mains Water temperatures for Oakland, CA

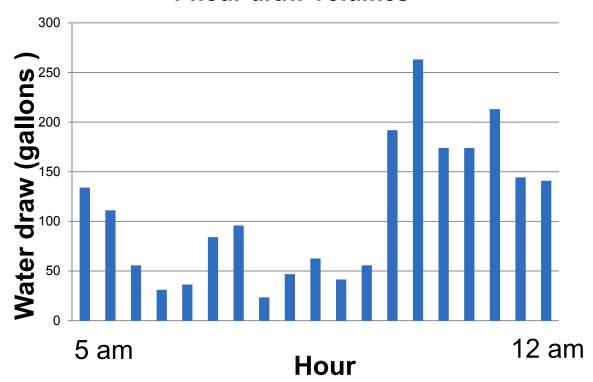


——Outdoor Air Drybulb Temperature [F](Hourly) ——Site Mains Water Temperature [F](Hourly)



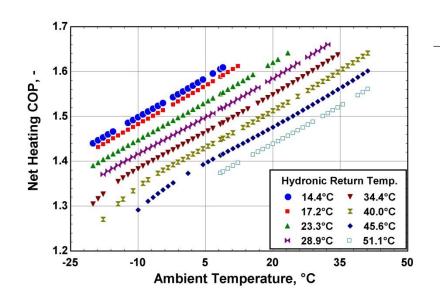
Daily draw pattern

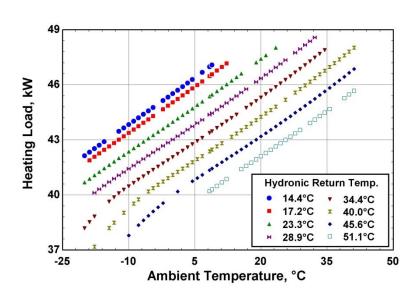




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GAHP COP and Heating Load as functions of Hydronic and Air Ambient Temperatures

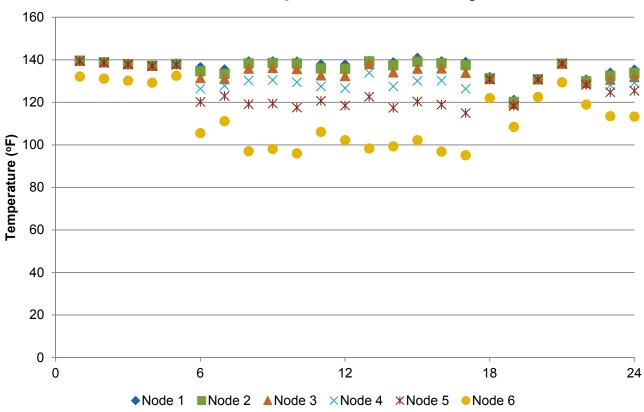






Tank Stratification

Nodal tank temperatures on May 18th

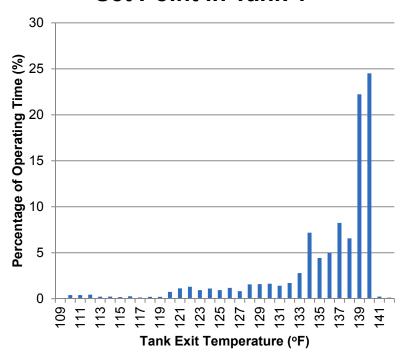




Performance Comparison

GAHP

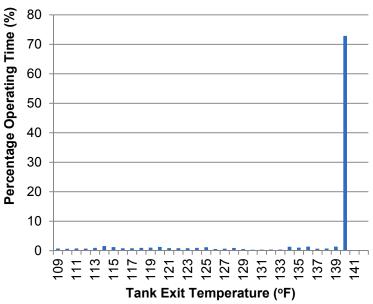
Achieving the Temperature Set Point in Tank 1



 Average daily consumption of 1104 ft³

Condensing Tank Pre-Heat

Achieving the Temperature SP in Tank 1



 Average daily consumption of 1638 ft³



Future Plans

- Investigate how each regional climate affects the performance
- Explore other water draw data resources
- Better understand the EnergyPlus HeatPump and Stratified models
- Model a water heating tank with internal heat exchanger coil



Thank You!



